# WASTE WATER PURIFICATION

# CURRENT TECHNOLOGY

Reverse Osmosis is and has been the mainstay of water purification for small and large scale applications in the USA. However, in the past fifty years a large research effort for water purification was directed at laboratory scale eutectic freeze crystallization and commercial scale freeze crystallization plants. Mostly GEA MESSO Gmbh Germany and GEA NIRO PT Netherlands have specialized in freeze crystallization techniques for more than just wastewater.

Typical GEA plants are shown in the following two photos:



GEA Spin bath regeneration plant



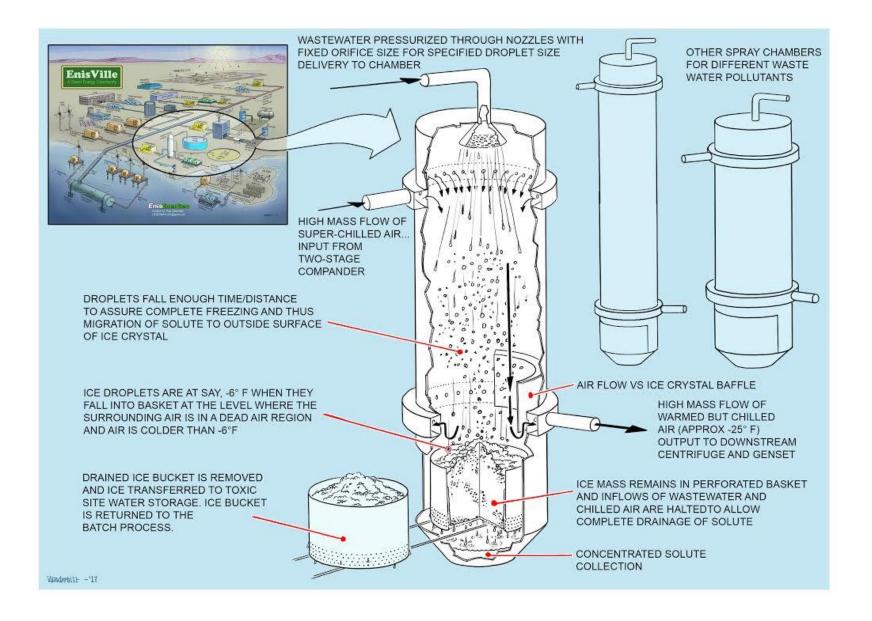
# GEA Research and development services and facilities for crystallizers

The above systems use bulk volume vats of wastewater, hour-long crystallization times and freezing temperatures associated with conventional refrigeration systems.

In the diagram next shown, the EEG LLC system uses sprayed (<1 millimeter ) droplets of waste water, few seconds long residence times and super-chilled air starting at -175°F at the top of the Freeze Crystallization Spray Chamber (FCSC) facility and warms to air at -6°F because of the heat exchange with the falling droplets. The droplets freeze and these brine coated ice

particles deposit as a porous frozen mass. The brine drains through the open channels in the deposited frozen mass of pure water.

#### INNOVATIVE TECHNOLOGY



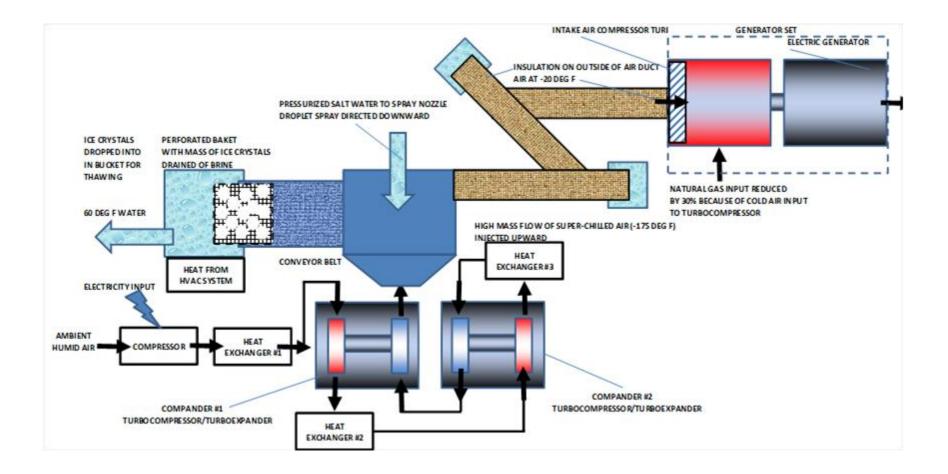
The outdoor spray chamber waste water purification system is more rugged and easy to operate than the shipboard indoor spray chamber salt water purification system because there is no need to fine tune the air speed in the outdoor version as carefully as the indoor version.

It is necessary to fine tune the droplet inject diameter so that it is small enough to freeze quickly (high surface area to volume) during its vertical drop in the chamber but large enough (small surface area to volume) to permit drainage of liquid brine from each droplet when it accumulates at the bottom of the chamber as well as a low packing factor to permit drainage in the open spaces in the accumulate mass of crystals at the bottom of the chamber.

It is necessary to make the cross-sectional area of the chamber as large as practical to slow the downward speed of the air. Too high air speed will cause the droplets to pass downward vertically in too short time so that freezing does not have time.

The residence time in the chamber requires not only time to freeze the droplets and also time to permit migration of the solute to the outside of the wastewater droplet.

The drained concentrated solution will also be further processed to recover materials for reuse locally or for other uses elsewhere.



# The ultimate facility will use the TL-CAES system

### to generate the required high mass flow of -175 deg F super chilled air

#### LIQUID NITROGEN PURCHASED AT ABOUT \$0.45/GALLON 480.000 GALLONS PER DAY OLLUTED POND WATER IN INSULATED PIPE TO AVOID FREEZING IN INSULATED SPRAYER 113,000 SCFM N2 @ -320 DEG F WALLS ARE MADE OF 2 X 4 WOOD FRAME WORK DRIVEN FRAMEWORK IS FILLED WITH 4 INCHES THICK FOAM FROM LIQUID NITROGEN VAPORIZOR (IGNORE HVAC AND GENSET APPLICATION) INSULATED FRAMEWORK ATTACHED TO FOUR VERTRICAL STRUCTURAL STEEL I-BARS SUPPORT WEIGHT WIND LOADING DROPLETS AT + 60 DEG F GN2 AT - 320 DEG F CHAMBER 6 FEET ABOVE GROUND FACILITATES REMOVAL OF AMASSED ICE (SNOW) IN BATCHES THROUGH THE DOOR AND THEN DOWNLOADING TO WAITING VEHICLE VIA SLIDE GN2 AT - 10 DEG F ICE (SNOW) REMOVED IN BATCHES . . 0 FRESH WATER FROM THAWED ICE 1:::: DROPLETS AT COLDER THAN FRESH WATER AT + 34 DEG F 1 10 DEG F FOR KCI SPRAYED AS WASH WATER . 1 -6 DEG FOR NaCl TO DISPLACE POND LIQUID 1÷ DOOR FROM DEPOSITED 13 LAYER OF ICE PARTICLES Т AFTER BOTTOM OF CHAMBER ACCUMULATES TALL CYLINDER OF ICE WITH CONE CAP PERFORATED AND IS DECANTED IN-PLACE. **1. ICE SENT TO THREE STAGES OF WASHERS** AND REMOVABLE 2. LIQUID CONCENTRATE SENT TO STORAGE BASKET FOR SUBSEQUENT MINERAL RECOVERY PLATFORM ALONGSIDE DOOR CONE OF GN2 AT 0 DEG F SLIDE CONNECTS POROUS DOOR TO WAITING VEHICLE PURE ICE CONCENTRATED AT POND WATER -6 DEG F

FIELD FACILITY FOR REMOVAL OF SALTS, ORGANIC AND OTHER POLLUTANTS FROM WASTE WATER

If higher purity is required, washing cycles are added as shown in the next diagram:

For laboratory testing vaporized liquid nitrogen is used to supply a small flow rate of super chilled gas. For large waste water streams a compander is used to supply the high mass flow of super-chilled air. For larger waste water streams the TL-CAES system supplies the high mass flow of super chilled air.

Note the simplicity of the facility. It has a small footprint, lightweight, not excessively tall, has no expensive machined parts and is portable.

The Dr. Dyllon Randall and others (see technical sections in this website) have shown that reverse osmosis followed by freeze crystallization is the most energy savings approach to purifying wastewater. The simple EFSC chamber will handle simple solutes.

For backup of the EFSC it is necessary to have three desk-top size EFSC chambers that are instrumented to provide design rules for the simple EFSC chamber in terms of adjusting design parameters so that more complex solutes can be handled.

The three desk-top size EFSC chambers that are heavily instrumented to provide backup for the simple EFSC chamber in terms of adjusting design parameters so that toxic solutes can be handled. The legal issues involved in offering potable water require a rigorous protocol.

The processing of wastewater from mining, agriculture and fracking is ideal for the FCSC facility. There are large droughtridden communities in the USA where these waste water streams need re-use. The EEG LLC solution offers a relatively inexpensive solution to large swaths of the USA.

Thermal energy storage system using compressed air energy and/or chilled water from desalination processes *T-CAES SYSTEMS, DESALINATION AND THERMAL ENERGY STORAGE (T.E.S.)* 

US 7,856,843 B2	October 23, 2006
Australian 2014202086	April 14, 2014
Chinese ZL200780046557.7	October 18, 2007
South Africa 2009/03446	October 18, 2009

Desalination method and system using compressed air energy systems

#### T-CAES OR TL-CAES SYSTEMS AND DESALINATION

US 8,695,360 B2	September 9, 2009
US 8,863,547	March 30, 2007
Australian 2007238919	March 30, 2008
South Africa 2008/09457	March 30, 2008

#### Desalination method and system using a Continuous Helical Slush Removal System

#### T-CAES SYSTEMS AND DESALINATION

US 2010-0018247 A1	July 24, 2006
Australia 2014202087	April 14, 2014
South Africa 2009/01223	February 20, 2009

Eutectic Freeze Crystallization Spray ChamberCAES SYSTEMS AND DESALINATIONUS 15/209,666 (pending)July 13, 2016